

REINHOLD ENVIRONMENTAL Ltd.



2019 NO_x-Combustion-CCR Round Table Presentation

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2019 NOx-Combustion-CCR/PCUG Conference

Impact of Air In-Leakage on Combustion, Emissions and Cost of Unit Compliance & Operation

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2019 NOx-Combustion-CCR/PCUG Conference

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Affordable Clean Energy (ACE) Rule

(EPA's replacement to the Clean Power Plan CPP)



Proposal: Affordable Clean Energy (ACE) Rule

On August 21, 2018, the U.S. Environmental Protection Agency proposed the Affordable Clean Energy (ACE) rule which would establish emission guidelines for states to develop plans

Related Actions

Proposes to reduce GHG emissions through four main actions:

- ACE defines the “best system of emission reduction” (BSER) for existing power plants as **on-site, heat-rate efficiency improvements**;
 - *Supports lower operating costs, improving competitiveness and dispatchability.*
- ACE updates the **New Source Review (NSR)** permitting program to further encourage efficiency improvements at existing power plants;
 - *Currently NSR is triggered when total annual emissions increases, penalizing efficiency improvements that would increase dispatchability. The update proposes NSR to be triggered when hourly emissions increase.*
- ACE provides states with a list of “candidate technologies” that can be used to establish standards of performance and be incorporated into their state plans;
- ACE aligns regulations under CAA section 111(d) to give states adequate time and flexibility to develop their state plans.

Opportunities to Resolve Air In-Leakage

- Boiler Dead Air Spaces

- Penthouse penetrations
- Header vestibules
- Nose arch
- Lower slopes
- Casing
- etc.

- In-situ Manufactured Expansion Joints

- Flue Gas Path
- Primary Air
- etc.

- HRSG's

- Penetrations
- Expansion Joints

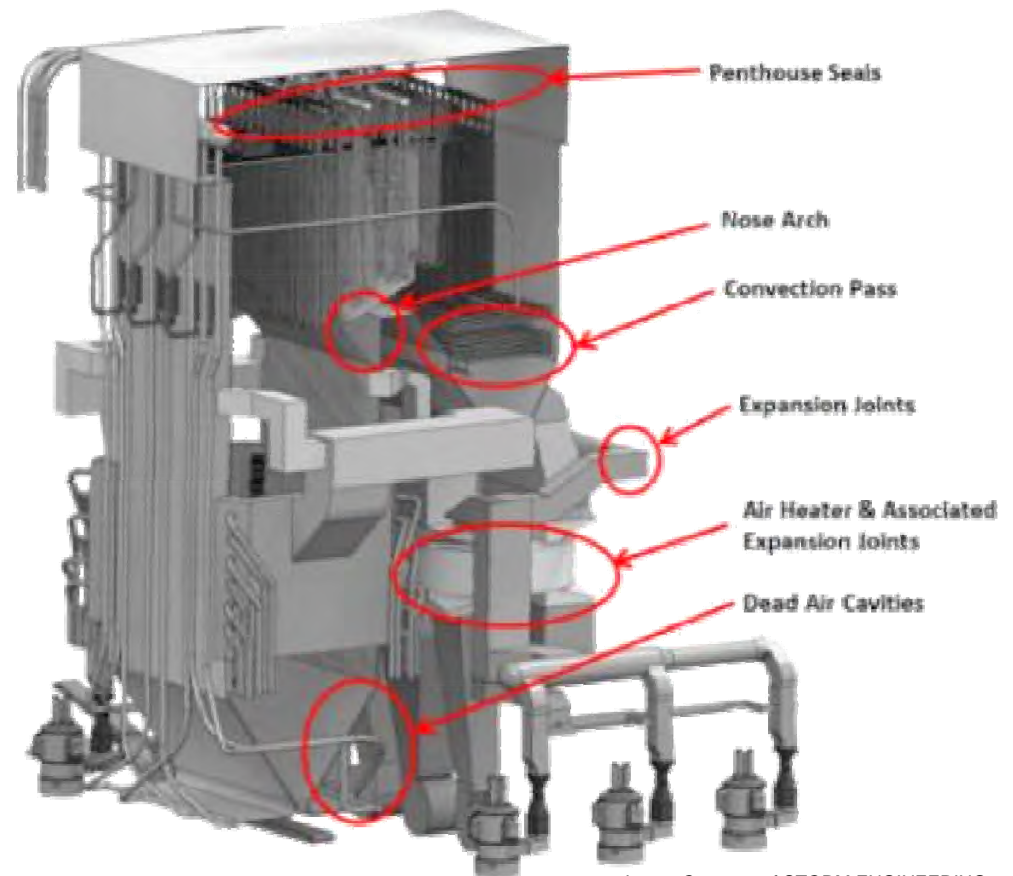
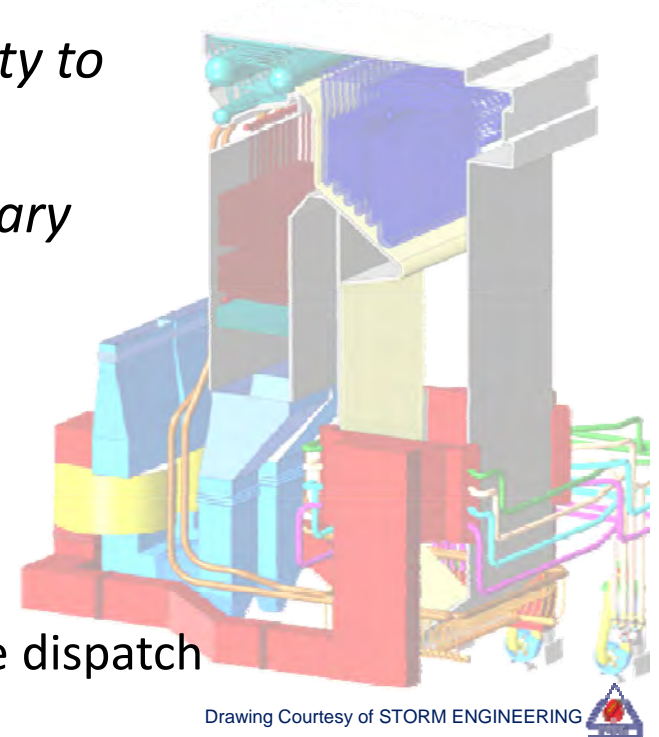


Image Courtesy of STORM ENGINEERING

Plant Financial Performance =

CRITICAL: Know the \$ value of each heat rate point

- + Heat Rate – *(lowest cost per saleable MW)*
- + Dispatchability – *(higher capacity factor > higher revenues)*
- + Optimize Capacity – *(net generation, reliability to avoid lost opportunity costs)*
- + Reduce Production Costs – *(fuel costs, auxiliary power consumption, sorbent costs)*
- + Emissions Compliance
- + Safety
- **All are Impacted by Air In-Leakage**
 - Made worse by increased cycling & unpredictable dispatch



Impacts of Air In-Leakage

- Heat Rate: (150-300 Btu/kWh effect common)
- Erroneous O₂ readings
- Efficiency: (*=improved profitability*)
 - Excess fuel consumption per Saleable MW
 - High LOI's (~25 Btu/kWh)
 - EGT: every 10°F over = (~25-30 Btu/kWh)
 - Parasitic power consumption
 - Fan limitations > loss of saleable MW, reduced capacity
- Reliability & Maintenance:
 - Increased slagging (~25 Btu/kWh)
 - Tube failure potential: accelerated tube wastage, overheating, clinker damage
 - Increased back-end corrosion
- Emissions:
 - (MATS compliance) Excess PM/per MMBtu
 - Sorbent consumption requirements

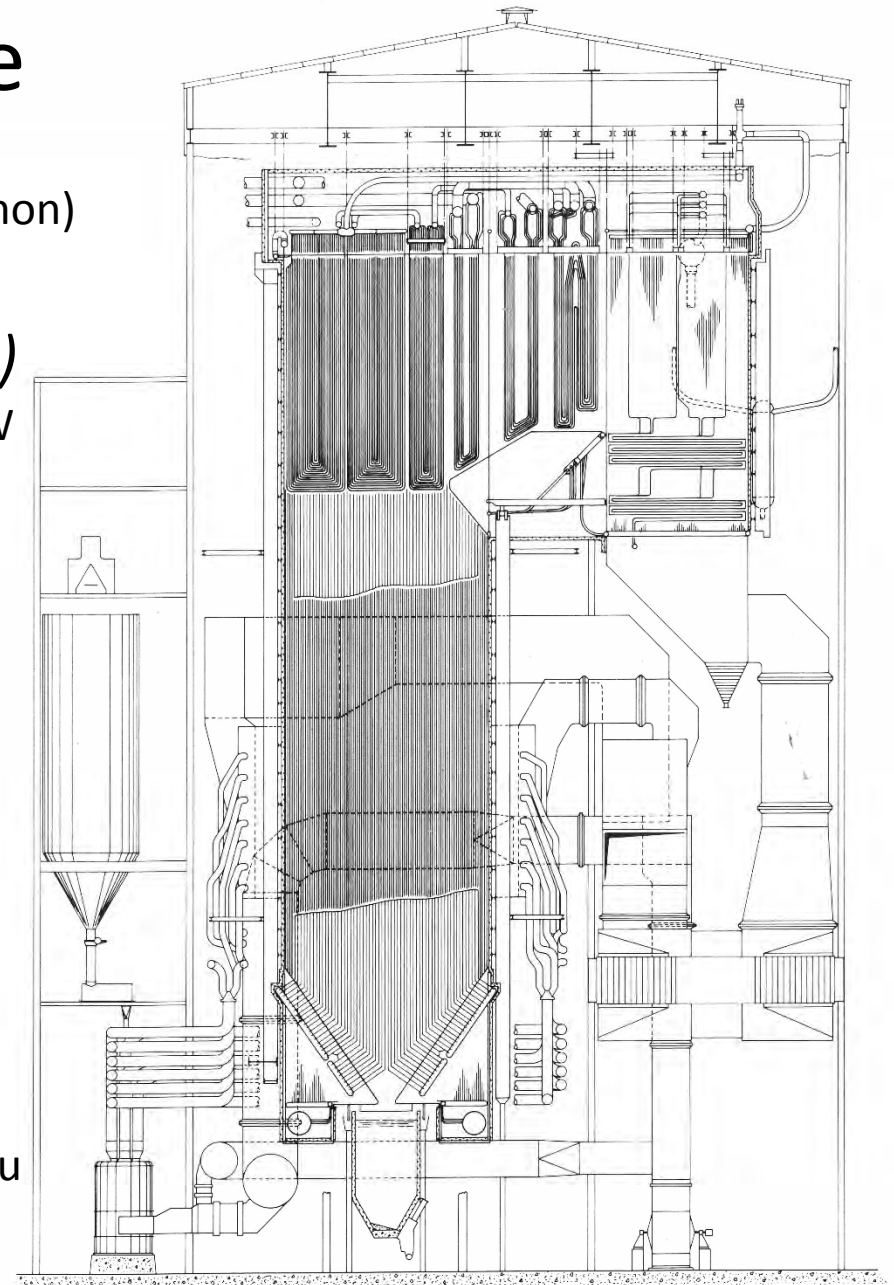


Image Courtesy of Combustion Fossil Power Systems



Environmental Impacts of Air In-Leakage

- **Excess Air**
 - Excessive NO_x emissions
 - Reduced combustion efficiency
- **Inaccurate O₂ Readings**
 - Higher fuel consumption = more throughput per BTU
- **Increased Gas Volume**
 - Can exceed the capacity of the APC equipment
- **Increased Gas Velocity**
 - Insufficient residence time
 - Poor gas flow distribution
- **Decreased Flue Gas Temperatures**
 - Reduces sorbent effectiveness
- **Increased Moisture**
 - Increases ash resistivity
 - Increases wetted particulate

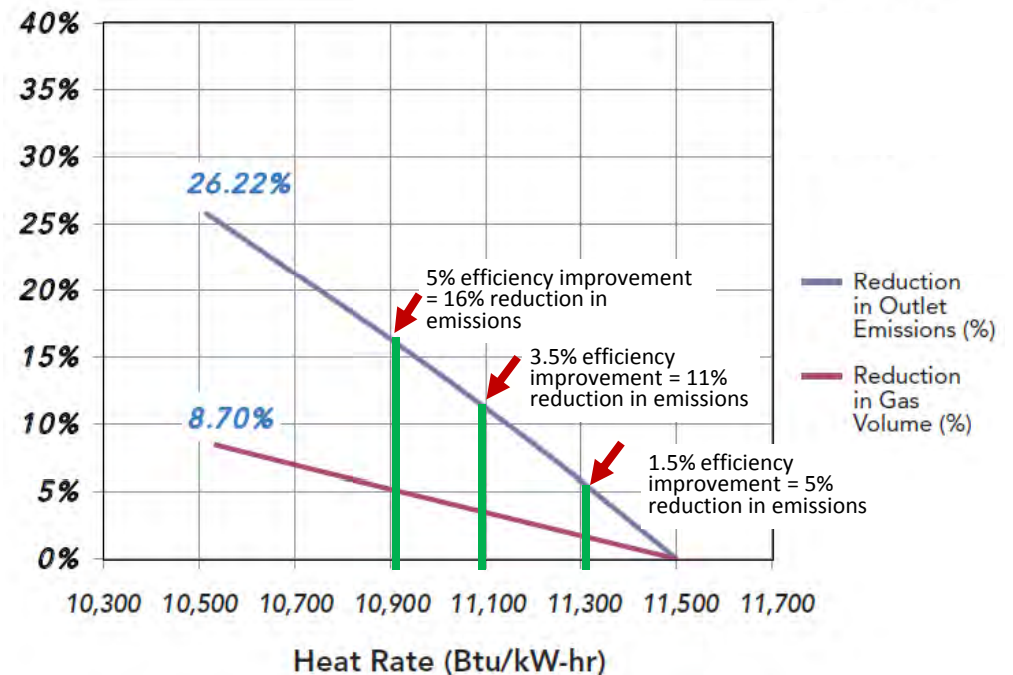


Boiler Thermal Efficiency and Emissions

- Improved Efficiency
= reduced gas volume
= reduction in outlet emissions

EXAMPLE: Minimizing air in-leakage is critical to improving unit efficiency. An improvement of 8.7% reduces throughput/gas volume (gv) the same, optimizing APC performance, reducing outlet emissions by ~26%.

- 5% gv reduction = 16% emissions reduction
- 3.5% gv reduction = 11% emissions reduction
- 1.5% gv reduction = 5% emissions reduction



Graph Courtesy of Neundorfer Inc. Particulate Knowledge

Data & Graph provided by Neundorfer, Inc.
"Boiler MACT Compliance: You Might be Closer Than You Think"

Flue Gas Temperature and Emissions

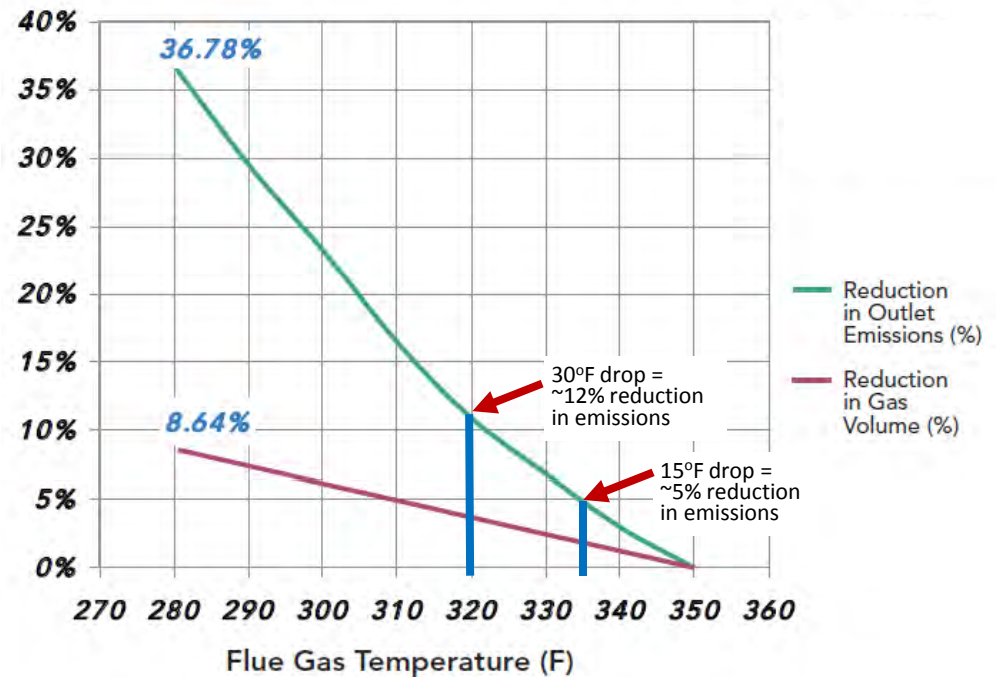
- Reduced Flue Gas Temperature = reduction in outlet emissions

EXAMPLE: As flue gas temperature is reduced from 350° to 280°, the gas volume is reduced by about 8.6%.

Ash resistivity and ESP performance are very sensitive to flue gas temperature.

By controlling flue gas temperature, outlet emissions were reduced by over 36%.

- 30°F reduction = 12% emissions reduction
- 15°F reduction = 5% emissions reduction



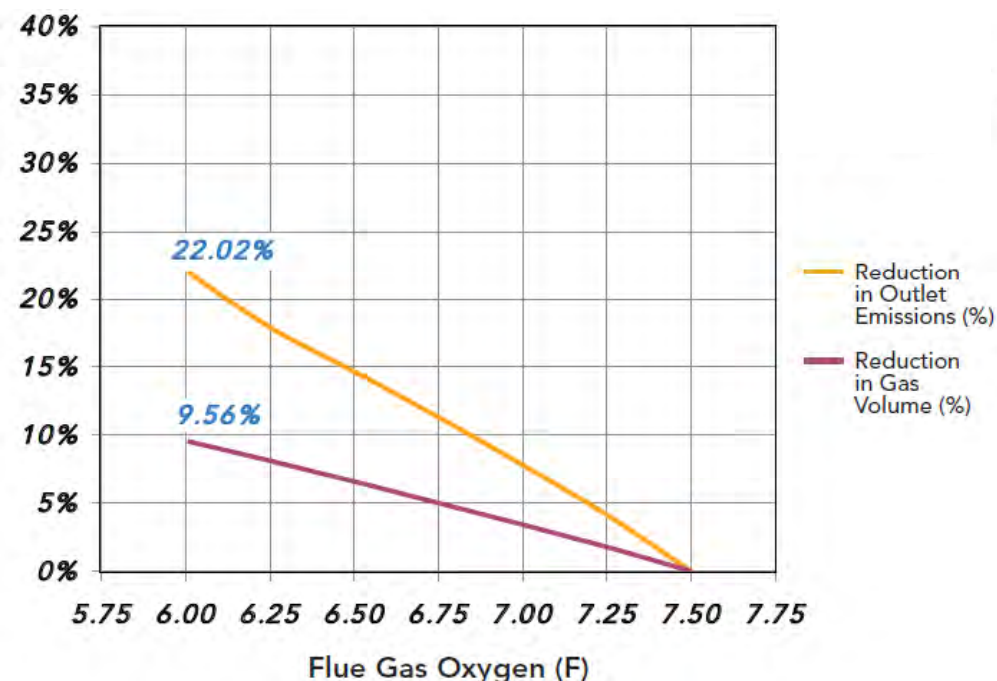
Graph Courtesy of Neundorfer Inc. Particulate Knowledge

Data & Graph provided by Neundorfer, Inc.
"Boiler MACT Compliance: You Might be Closer Than You Think"

Flue Gas Oxygen and Emissions

- Reduced air in-leakage/tramp air = reduced stack O₂ concentration = reduction in outlet emissions

EXAMPLE: Reducing the stack O₂ concentration from 7.5% to 6% reduced the treated gas volume by ~9.5%, resulting in a ~22% reduction in outlet emissions.



Graph Courtesy of Neundorfer Inc. Particulate Knowledge.

Data & Graph provided by Neundorfer, Inc.
"Boiler MACT Compliance: You Might be Closer Than You Think"

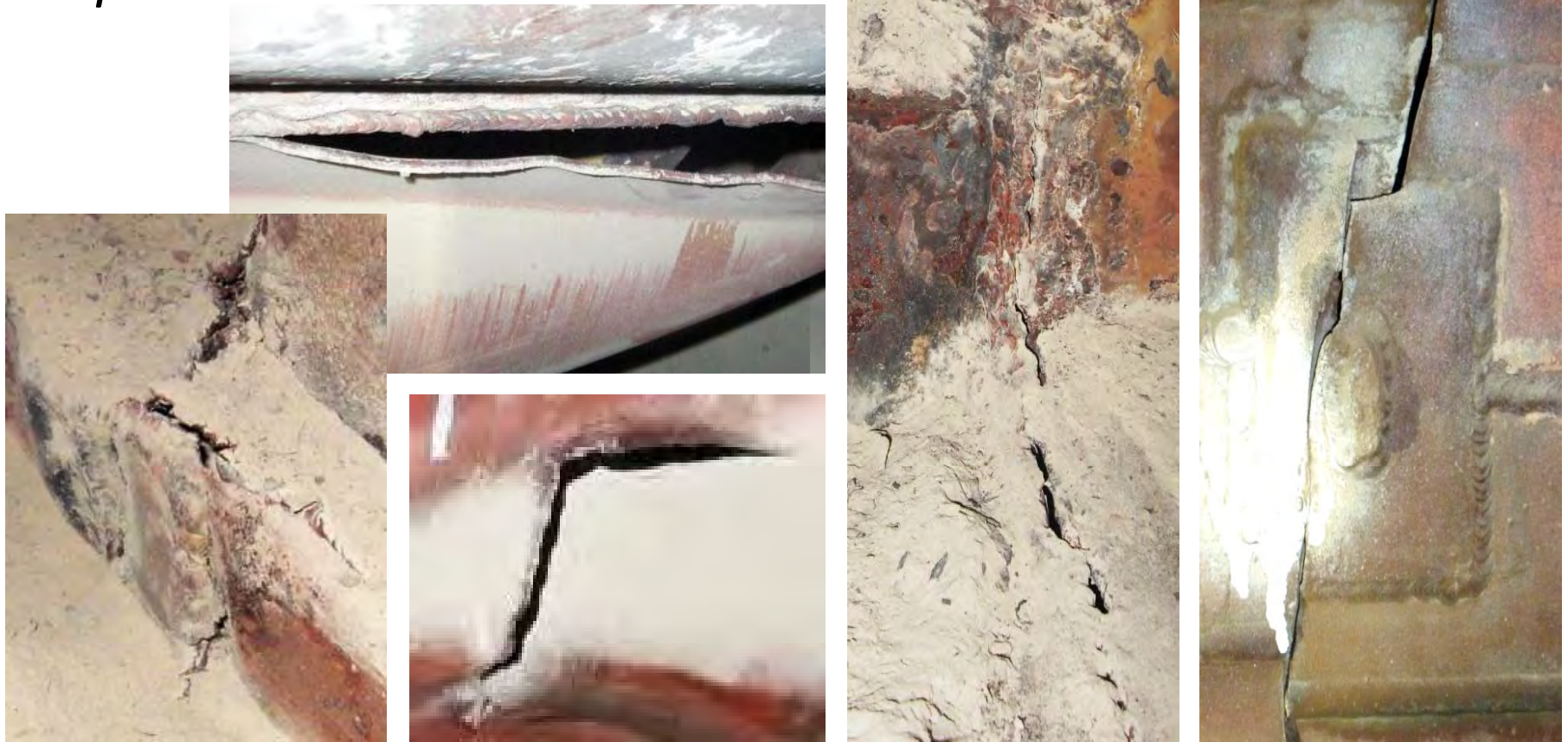
Cycling, Fractures, Corrosion = Air In-Leakage

- Average age of coal-fired is 40+ years old – Designed for baseload
- Mechanical damage
 - stress fractures
 - weld cracking
 - refractory failure
 - corrosion
 - Erosion



Traditional Options: **Weld Repairs**

- *Tend to re-crack at the heat affected zone of the weld repair, requiring repetitive repairs*



Traditional Options: Refractory

- *Lack of reliability can cause sudden spikes in excess air that can jeopardize unit performance and efficiency.*

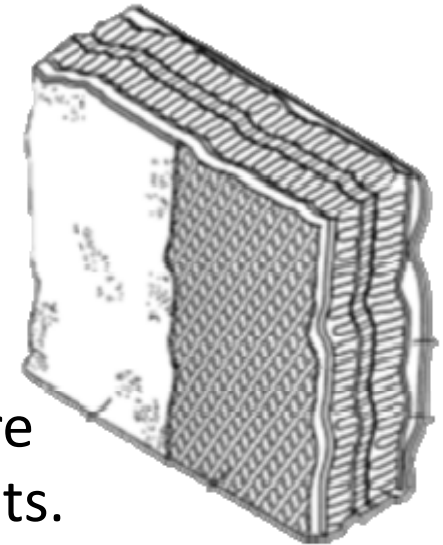


NEEDED: Sealing Method that's Compatible with Boiler Operation and Cycling

- High temperature threshold
- Malleable: Resilient in multi-plane movement, cycling environments
- Reliable: Maintenance-free, long-term sealing capability to reduce repetitive repairs and damage control
- Adaptable & rapid in-situ fabrication



Development of a Flexible, High Temperature Sealing System



- ISOMEMBRANE: Designed to remain flexible, handling multi-plane movement in high-temperature (1,800°F), cycling and variable pressure environments.
 - Boiler Dead Air Dead Spaces
 - Expansion Joints

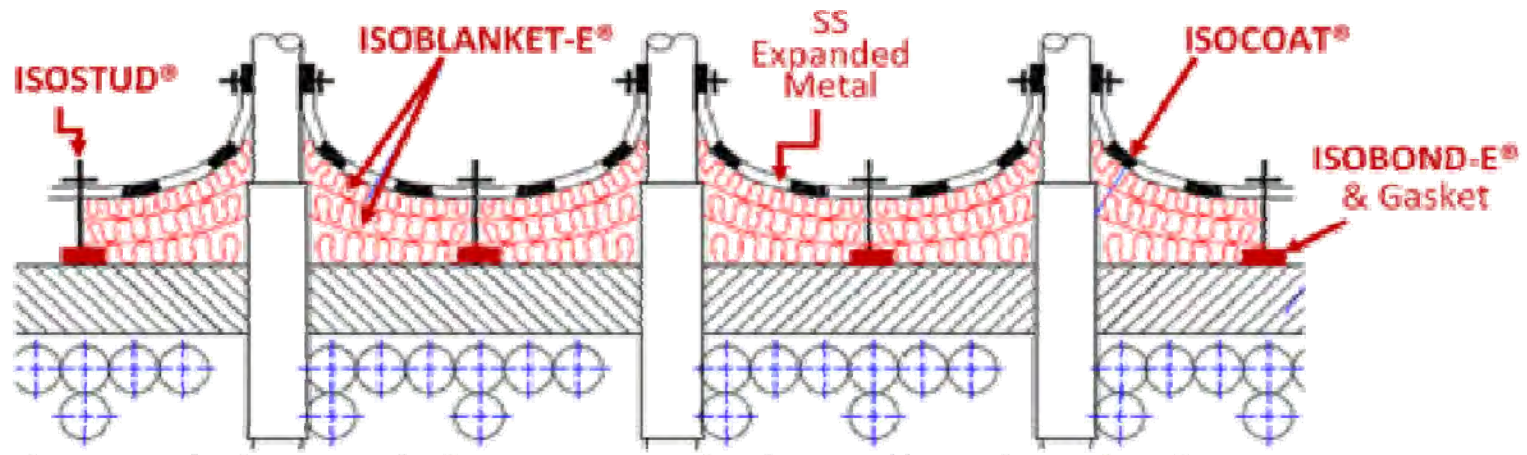
(1) United States Patent
Gelsome et al.
(10) Patent No.: US 8,590,504 B2
(15) Date of Patent: Nov. 26, 2013

(54) HIGH TEMPERATURE SEAL
(71) Applicant: Hask Brands, LLC, Charlotte, NC (US)
(72) Inventor: Andrew C. Gelsome, Charlotte, NC

(50) Field of Classification Search
USPC 289/003, 890/011, 402/02, 402/06,
289/012, 277/626, 627, 650-654
See application file for complete search history.

- 1982: Developed in Denmark for boiler dead air space
- 1993: HTT introduced ISOMEMBRANE® to North America
 - 4 proprietary components (w/13-15 stages in the installation process)
 - 2 patents for seal construction
- 1995: Developed in-situ manufactured expansion joint encapsulations
- 2019: Over 2,500 North American installations since 1993

ISOMEMBRANE[®] Sealing System



Multi-layered system of several proprietary developed components:

- ISOBOND-E[®]: high strength, high temperature adhesive
- ISOBLANKET-E[®]: high tensile strength, high temperature blanket
- ISOCOAT[®]: protective topcoat sealing layer
- ISOSTUD[®]: stud design that increases seal attachment uniformity to ~99%, & reduces installation time ~10%
- These components work in unison to optimize sealing by merging flexibility, impermeability and robustness

ISOMEMBRANE® as a Tool

Boiler Dead Air Space Applications

- A maintenance-free alternative to refractory and weld repairs
- Provides reliable crack & penetration sealing service-life that typically lasts the life of the tubes



Boiler Installation Overview

example:
**Header Vestibule
Installation**



Case Study: 770MW CE Boiler – 1972

Air In-Leakage Reduction Project: December 2017

Penthouse: comprehensive sealing over the furnace
Flue Gas Path: 5 in-situ manufactured expansion joints

Snapshot Results:

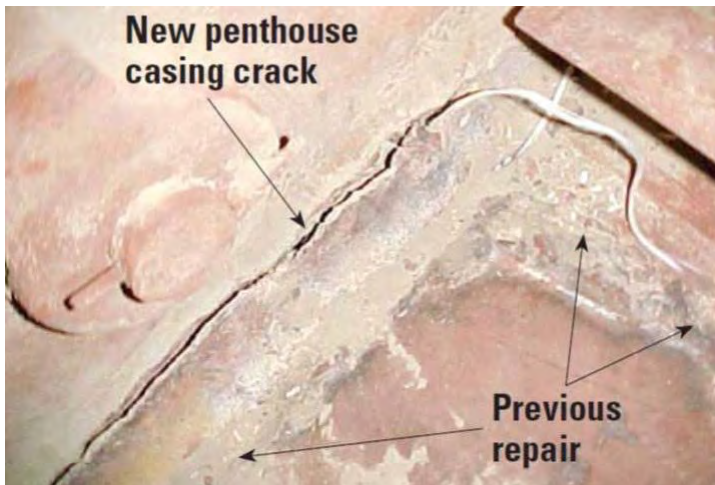
- Heat Rate improved
- Fully dispatched
- Excess O₂: dropped ~0.6%
- 2 de-slugging outages avoided
- FEGT Reduced 8.5°F
- Reduced aux power consumption
- Plus, other improvements



First year savings: \$3,180,671 - ROI 2.8 months

Case Study: Background

1999 ISOMEMBRANE Installation-PH over the Backpass

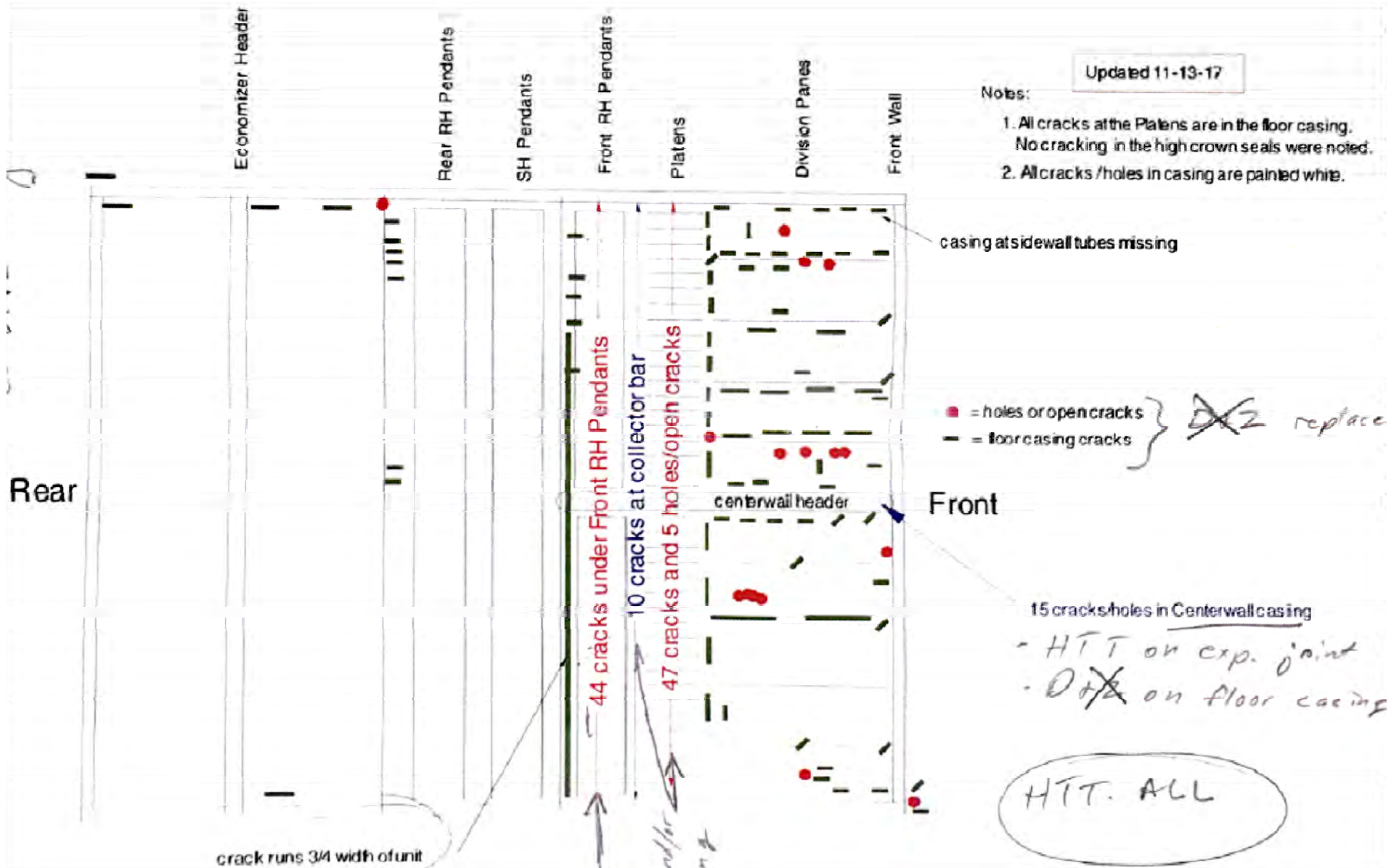


Images Courtesy of POWER Magazine & Innovative Combustion Technologies, Inc.

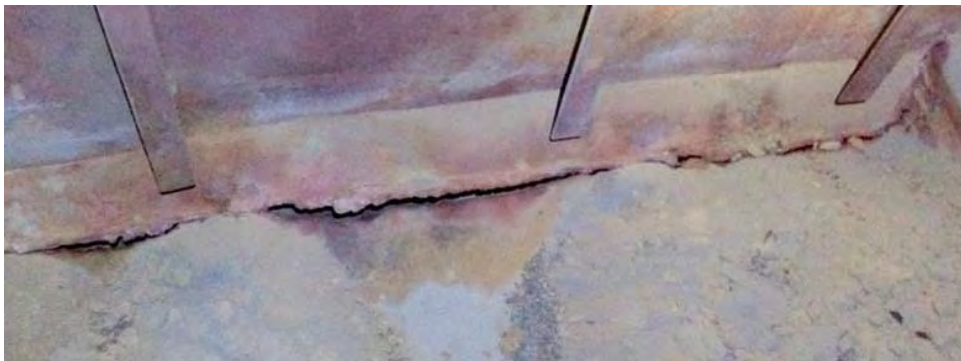
Case Study: ISOMEMBRANE® Reliability 2017 - after 18 years in-service – Still sealing, no maintenance required



Case Study: Inspection Map



Case Study: Penthouse Inspection



Case Study: Penthouse Inspection



Case Study: Penthouse Inspection



Case Study: ISOMEMBRANE® Scope Penthouse - Over the Furnace



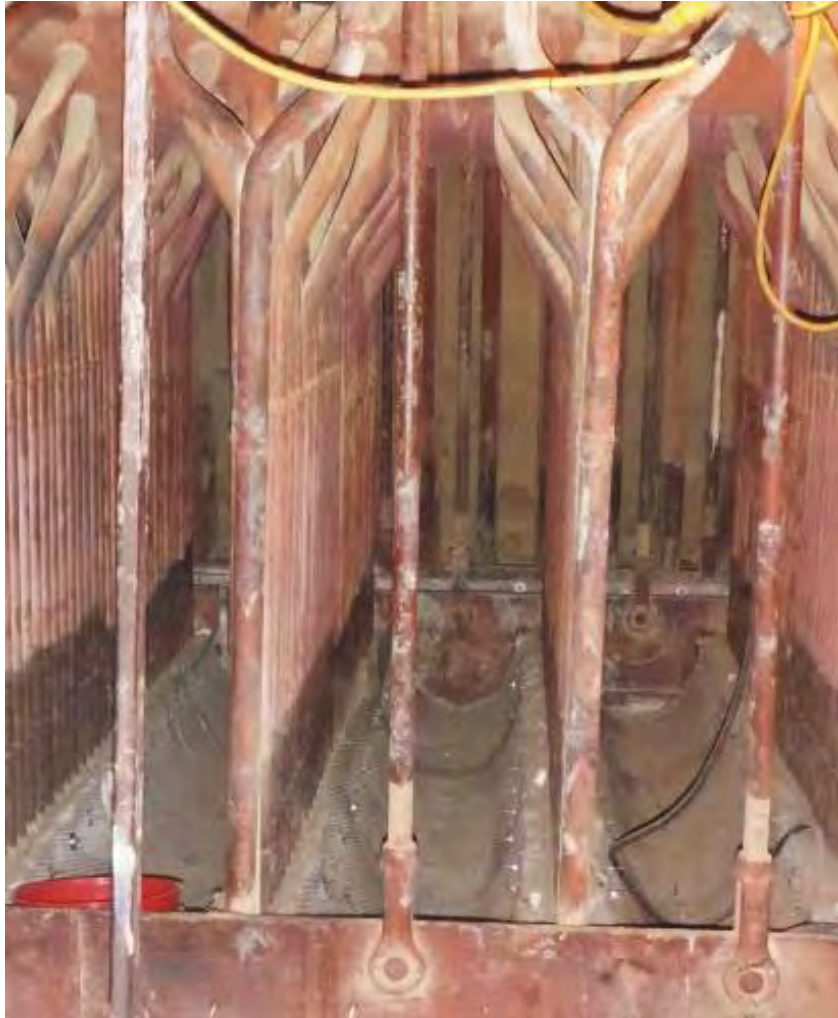
Case Study: Boiler Sealing Project Timeline

- 4,291 sq/ft - Completed in 13 shifts

Gorgas Steam Plant - December Outage - ISOMEMBRANE® Installation				Actual Start		In-Progress		Actual Completion																
HIGH TEMPERATURE TECHNOLOGIES, Inc. - 704-375-2111				10%: S=Stud		25%: G=Gasket		40%: B=ISOBlanket1		60%: BB=ISOBlanket2		80%: X=HexMetal		90%: SC=Secured										
Project Schedule				MON	TUES	WED	THUR	FRI	SAT	SUN	MON	TUES	WED	THUR	FRI	SAT	SUN	MON	TUES	WED	THUR			
Line/Area	DESCRIPTION			Sq/Ft	Lin/Ft	11/27	11/28	11/29	11/30	12/1	12/2	12/3	12/4	12/5	12/6	12/7	12/8	12/9	12/10	12/11	12/12	12/13	12/14	
PENTHOUSE				DAYS TO FINISH BOILER:		17	16	15	14	13	12	11	10	9	8	7	6	5	4	3	2	1		
7/A	X	OFFLINE	Penthouse Center Wall Header Expansion Joint (2 sides, 33 lf ea.)	132	66									50%										
7/B	X	OFFLINE	Penthouse Center Wall Casing at Floor (2 sides, 31.5 lf ea.)	189	63									50%										
7/C1	X	OFFLINE	Doghhouse 1 Penthouse North Furnace "A" Division Panel	88	44																			
7/C2	X	OFFLINE	Doghhouse 2 Penthouse North Furnace "A" Division Panel	88	44																			
7/C3	X	OFFLINE	Doghhouse 3 Penthouse North Furnace "A" Division Panel	88	44																			
7/C4	X	OFFLINE	Doghhouse 4 Penthouse North Furnace "A" Division Panel	88	44																			
7/D1	X	OFFLINE	Doghhouse 1 Penthouse South Furnace "B" Division Panel	88	44																			
7/D2	X	OFFLINE	Doghhouse 2 Penthouse South Furnace "B" Division Panel	88	44																			
7/D3	X	OFFLINE	Doghhouse 3 Penthouse South Furnace "B" Division Panel	88	44																			
7/D4	X	OFFLINE	Doghhouse 4 Penthouse South Furnace "B" Division Panel	88	44																			
7/E	X	OFFLINE	Penthouse North Furnace "A": Support Hanger Division Panel Side	74	32																			
7/E	X	OFFLINE	Penthouse South Furnace "B": Support Hanger Division Panel Side	74	32																			
7/F	X	OFFLINE	Penthouse North Furnace "A": Side Wall Header Casing (2 sides, 31 lf ea.)	93	62																			
7/H (no "G")	X	OFFLINE	Penthouse South Furnace "B": Side Wall Header Casing (2 sides, 31 lf ea.)	93	62																			
7/I	X	OFFLINE	Penthouse Front Water Wall Header (2 sides, 74 lf ea.)	222	148																			
7/J	X	OFFLINE	Penthouse Furnace Penthouse Floor Expansion Joint	110	74																			
7/K	X	OFFLINE	Penthouse Superheater Penetrations Inlet & Outlet Platens (40 bays)	1200	na																			
7/L	X	OFFLINE	Penthouse Reheat Penetrations Inlet & Outlet Platens (100 bays)	1400	na																			
Total Boiler Square Footage				4291																				

- The plant estimated repairing the same boiler scope with weld repairs and refractory would have required 52 shifts.

Case Study: Installation Penthouse – Over the Furnace



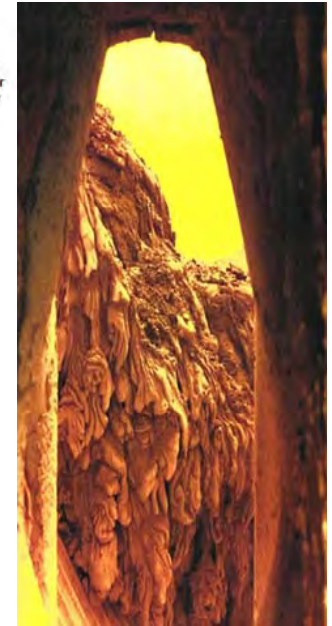
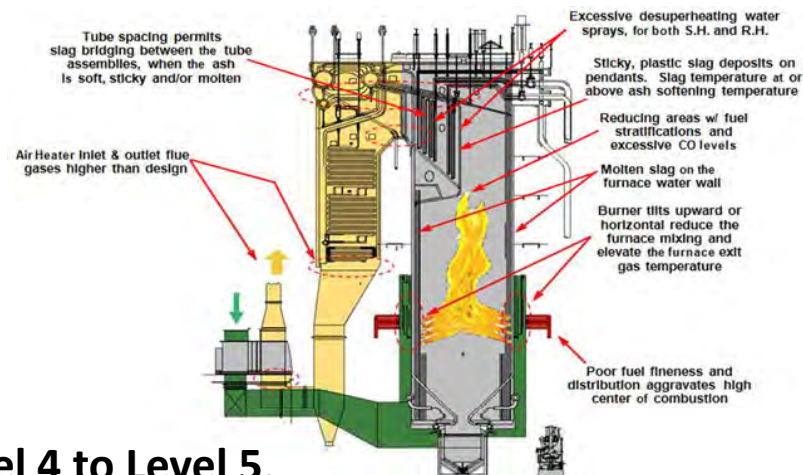
Case Study: Installation Penthouse – Over the Furnace



Case Study: Installation Penthouse – Over the Furnace



CASE RESULTS: OPERATIONAL ROI



1. Improved Heat Rate: From a Level 4 to Level 5. Best Heat Rate of the utility's coal-fired units

- *(In addition to ISOMEMBRANE® sealing the boiler and joints, the plant did some condenser, boiler trough, tube membrane and fan blade repairs.)*

2. Fully dispatched: Previously load-following.

3. De-slagging outages have been reduced 50% since returning to service. Previously this unit typically required 3-5 de-slagging outages per year, with each outage having a duration of 42-48 hours each.

4. Boiler air control is vastly improved: Excess O₂ reduced 0.6%

Before sealing: Excess O₂ = 3.8-4.0%, After sealing: Excess O₂ = 3.2-3.4%.



- Operators had to "reteach themselves how to run the unit"
- No longer have to "fudge" O₂ settings
- Before sealing, boiler air in-leakage was measured at 17%. Currently ~3%.

5. Excess fan capacity: Parasitic power consumption reduced.

6. Reduction in LOI: Estimated, 1% reduction.

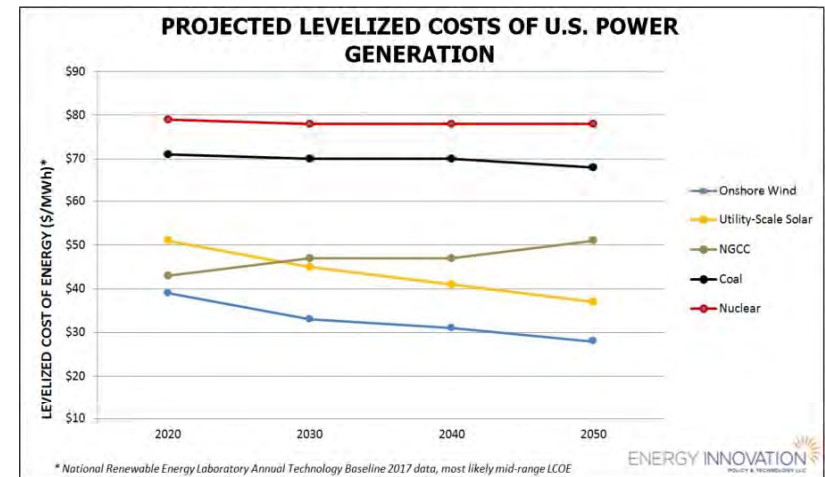
7. Opacity Reduction: 27%

CASE RESULTS: BOILER ROI Calculator

	A	B	C	D	E	F	G	H	I	J		
1												
2	 <p>The Boiler ROI calculator was created for HTT by INNOVATIVE COMBUSTION TECHNOLOGIES (ICT). ICT specializes in addressing combustion side parameters to identify & explore opportunities for improved unit heat rate, performance, availability, capacity and operability.</p>	 <p>High Temperature Technologies, Inc. 4324 Barringer Drive #107, Charlotte, NC 20817 704.375.2111 www.isomembrane.com Patrick Fitzgerald cell: 704.621.2465 patrick@isomembrane.com</p>	<p>Yellow Boxes are for manual data entry. Other fields self compute.</p>									
3			<p>For a copy of this BOILER ROI Calculator (in Excel format), email patrick@isomembrane.com, and I'll send you a copy.</p>									
4												
5												
6												
7	ROI Calculator - Air In-Leakage Control											
8	Unit Net Load (Mw)	770			Hours/yr	6570						
9	Availability	75%			Capacity Factor	75%						
10	Number of ID Fans	4			Fan HP	6,000						
11	Heat Rate (Btu/Kwhr)	8,691	2017 - 9,820		Heat Rate (Btu/Mwhr)	8,691,000						
12	Fuel Cost (\$/ton)	\$51			Fuel Heating Value (HHV) Btu/lb	12,000						
13												
14	Calculations:											
15	MW's/year - MW's/year= Unit Net Load (Mw) * Cap Factor (%) * 365 (days/yr) * 24 (hrs/day)		3,794,175	Total MW's								
16	Fuel Cost											
17	\$/MMBtu = Fuel Cost (\$/ton) * 1,000,000 / (HHV (Btu/lb) * 2000 (lb/ton))		\$ 2.13	\$/MMBtu								
18	\$/MwHr = (Heat Rate (Btu/MwHr) * Fuel Cost (\$/ton)) / (Heating Value (Btu/lb) * 2000 lb/ton)		\$ 18.47	\$/MwHr			Estimated Annual Saving from Reduced Sorbent Consumption, ESP Power, Fuel Efficiency, etc.:	\$ 250,000				
19												
20	Parameter		Quantity or % Change in Heat Rate	Sale Price or Penalty	Total Cost Savings (per year)	Savings LOW	Savings HIGH					
21	FLYASH LOSS ON IGNITION (LOI) (alternative way of looking at fuel savings)		1 % Reduction in LOI	8.69 Btu/KwHr	\$ 70,072	\$ 70,072						
22	(Assume 0.1% Heat Rate per 1% LOI)		2 % Reduction in LOI	17.38 Btu/KwHr	\$ 140,144		\$ 140,144					
23												
24	LOST GENERATION	Occurrences/yr	Hours/occ		\$/Mwhr							
25	Lost Generation (54Mw de-rate to shed furnace slag)	0	8		\$25	\$ -	\$ -					
26	Lost Generation (54Mw de-rate to shed furnace slag)	0	8		\$25	\$ -	\$ -		\$ -			
27	Lost Generation (Unit off-line due to slugging incident, (x) 3-day incidents/yr)	2	42		\$25	\$ 1,617,000	\$ 1,617,000					
28	Lost Generation (Unit off-line due to slugging incident, (x) 3-day incidents/yr)	3	42		\$25	\$ 2,425,500		\$ 2,425,500				
29	Plus fuel oil for restarts	2	41,000	\$4.15	gallon		\$ 340,300					
30												
31	REDUCED AUXILIARY HORSEPOWER FOR ID FANS											
32	(Repair resulted in decrease in mass flow of ~4%) yielding ~ reduction in ID hP of 10%	600.00		# ID Fans * Capacity factor * HP Reduction * .7455 Kw * Yearly Hours	\$0.045 KwHr/Bus Bar cost	\$ 396,733	\$ 396,733					
33	(Repair resulted in decrease in mass flow of ~8%) yielding ~ reduction in ID hP of 20%	1200.00		# ID Fans * Capacity factor * HP Reduction * .7455 Kw * Yearly Hours	\$0.045 KwHr/Bus Bar cost	\$ 793,465		\$ 793,465				
34												
35	DE-SUPERHEATING SPRAY FLOWS (SH) Assume 0.025% Heat rate for 1% of MSF	1	1 % MSF Sprays Reduced		2.17 Btu/KwHr	\$ 17,518	\$ 17,518					
36	De-superheating Spray Flows (SH) Assume 0.025% Heat rate for 1% of MSF	2	2 % MSF Sprays Reduced		4.35 Btu/KwHr	\$ 35,036		\$ 35,036				
37												
38	DE-SUPERHEATING SPRAY FLOWS (RH) Assume 0.2% Heat rate for 1% of MSF	1	1 % MSF Sprays Reduced		17.38 Btu/KwHr	\$ 140,144	\$ 140,144					
39	De-superheating Spray Flows (RH) Assume 0.2% Heat rate for 1% of MSF	2	2 % MSF Sprays Reduced		34.76 Btu/KwHr	\$ 280,289		\$ 280,289				
40	*MSF (Main Steam Flow)											
41												
42	REDUCED BOILER EXIT GAS TEMPERATURE (.25% change in heat rate per 10°F)		8.5 °F Reduction		18.47 Btu/KwHr	\$ 148,904	\$ 148,904					
43	AH A Gas Out: 335F (2017) to 324F (2018) / AH B Gas Out: 319F (2017) to 313F (2018)		20 °F Reduction		43.46 Btu/KwHr	\$ 350,361		\$ 350,361				
44	COST OF FUTURE MAINTENANCE ACTIVITIES AVOIDED	Low	High									
45	Penthouse Vacuuming	\$ 15,000	\$ 20,000				\$ 15,000	\$ 20,000				
46	Refractory Redo/Repairs	\$ 25,000	\$ 40,000				\$ 25,000	\$ 40,000				
47	Penthouse casing/penetration weld repairs	\$ 60,000	\$ 120,000				\$ 60,000	\$ 120,000				
48							\$ 100,000	\$ 180,000				
49												
50	Cost: Unit 10 ISOMEMBRANE® Applications : PH over furnace, ESP Inlet XJ's, AH Inlet XJ's & FGD Duct XJ		\$ 733,725	ROI (Months): 2.8		Annual Potential Savings Total	\$ 2,930,671	\$ 4,384,796				
51	CONFIDENTIAL: This document and calculator are for internal use only.											
52							\$ 3,180,671					
53												

CASE RESULTS: FINANCIAL ROI

\$3,180,671 annual savings
Project ROI 2.8 months



1. **Avoided 2 de-slagging outages (average 42 hours each):** In the 9 months following the installation, zero de-slagging outages had been required. **Current Savings: \$1,617,000**
Annual savings: \$2,482,200 - \$3,309,600/year
2. **Start-up Fuel Oil Reduction:** 41,000 gallons at \$4.15/gal = \$170,150 x 2 = **\$340,300**
3. **Reduced Fan Auxiliary Power Consumption: \$396,733**
4. **Reduced de-superheating (RH & SH) spray flows: \$157,662**
5. **Reduction in dry gas loss and FEGT: \$148,904**
6. **Reduction in LOI: 1% reduction = \$70,072**
7. **Repetitive maintenance avoided:** Estimated, **\$100,000-\$180,000**
8. **Other financial improvements:** Additional savings from reduced sorbent consumption, corrosion, ESP power consumption, & improved fuel efficiency. Estimated, **\$250,000-\$350,000**

(Based on results data provided by the plant or estimated based on experience with hundreds of boilers by HTT, Innovative Combustion Technologies and Storm Engineering.)

CASE RESULTS: MAINTENANCE ROI

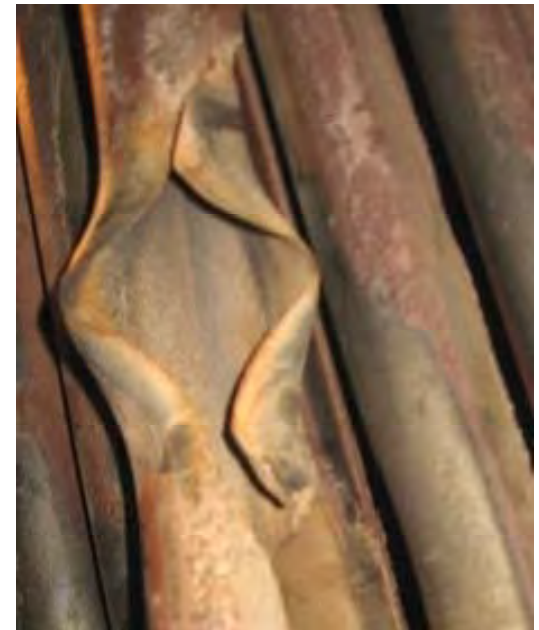
1. **ISOMEMBRANE®** was less than half the cost than traditional repair methods, and 3x faster to install.
2. **Reduction or elimination of repetitive weld & refractory repairs, and vacuuming.**
 - Reduced annual repairs equals reduced welder & boiler-maker requirements, freeing up quality welders/workers to focus on more critical applications
3. **Reduced safety risks:** fewer workers on-site, less hot work, fewer vacuum hoses, etc.



CASE RESULTS:

RELIABILITY/EFOR ROI

- 1. Reduced potential for boiler tube wastage and forced outages.**
 - Air in-leakage allows for sub-stoichiometric conditions. As plants are experimenting with different fuels (especially Illinois Basin), it's common to see wastage rates increase to 80 mpy.
 - The average lost opportunity cost of each tube leak for this plant is ~\$950,000 - ~\$1,450,000. (If ash has accumulated, delays to access to repair can occur.)
- 2. Reduced propensity for slagging and/or clinker falls.**
- 3. Reduced propensity for secondary combustion.**



Case Study: Duke Marshall Penthouse

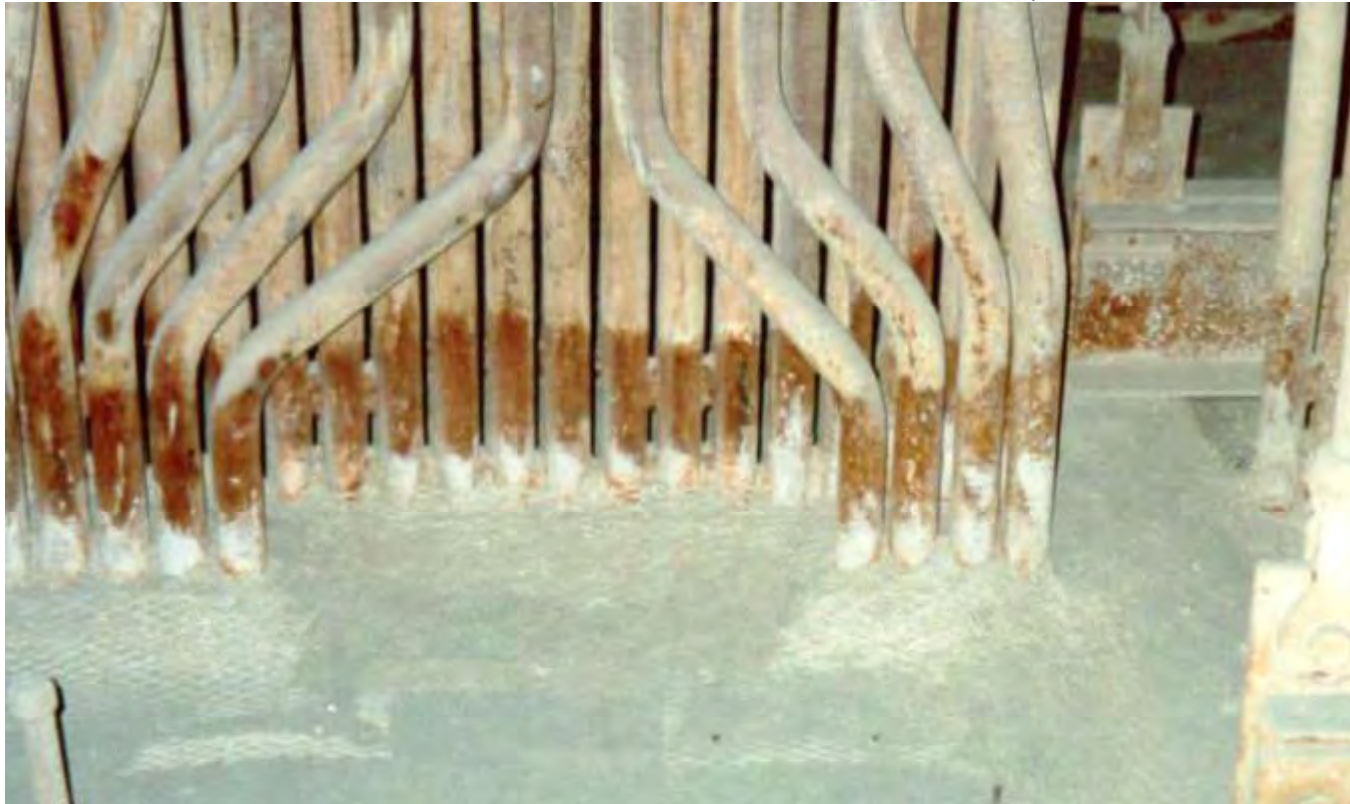
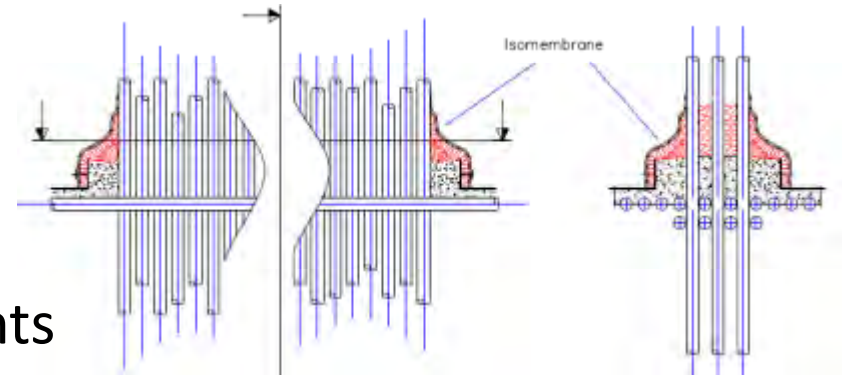
- Unit 4: 700 MW Supercritical Unit
- 3-5 feet of ash accumulation
 - approximately 100 tons
- Ingress of flyash caused typical problems
 - Safety
 - Reliability
 - Efficiency
 - Housekeeping



***Prior to installation of
ISOMEMBRANE® in 1994***

Case Study: Duke Marshall Penthouse *After 1 Year in Service*

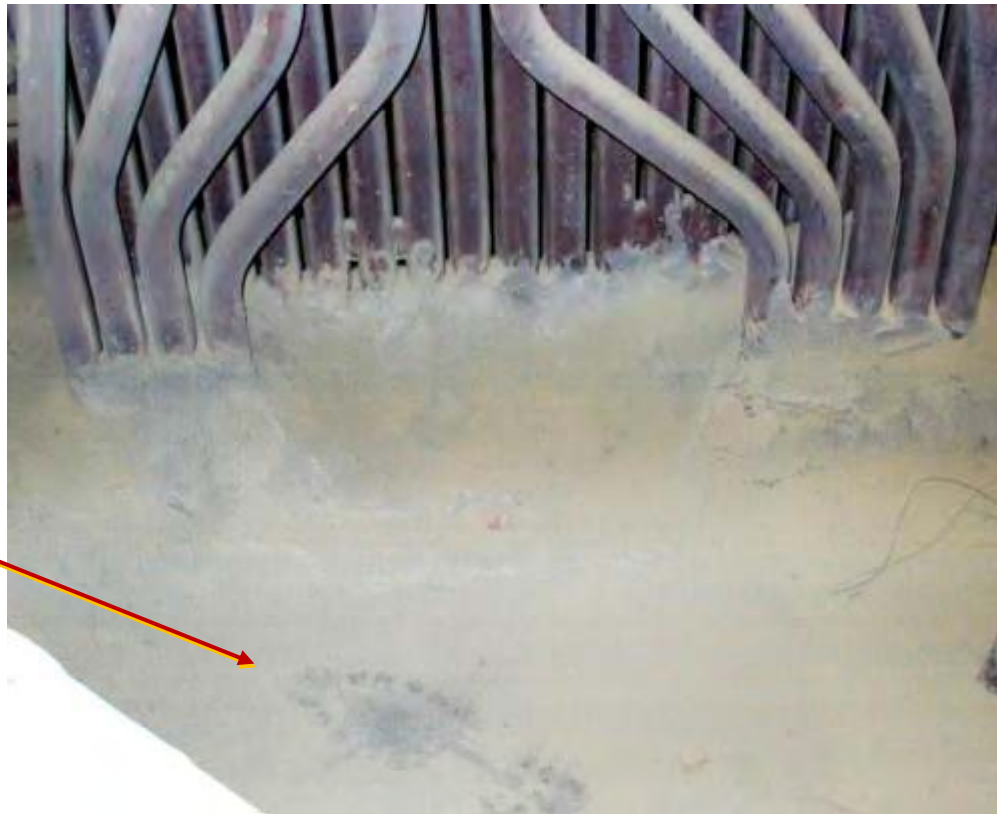
- No vacuuming required
- Reduced outage requirements
- Reduced costs and labor requirements



Case Study: Duke Marshall Penthouse *After 10 Years in Service*

- Still no vacuuming required, only minor ash dusting exhibited
- Improved outage costs, budget flexibility, labor and safety
- Significant payback in reduced vacuuming & inspection costs alone

*Minor ash dusting
(note foot print)*



Case Study: Duke Marshall Penthouse

After 16 Years

- No ISOMEMBRANE® maintenance required
- Improved outage effectiveness, safety, and time & budgetary savings



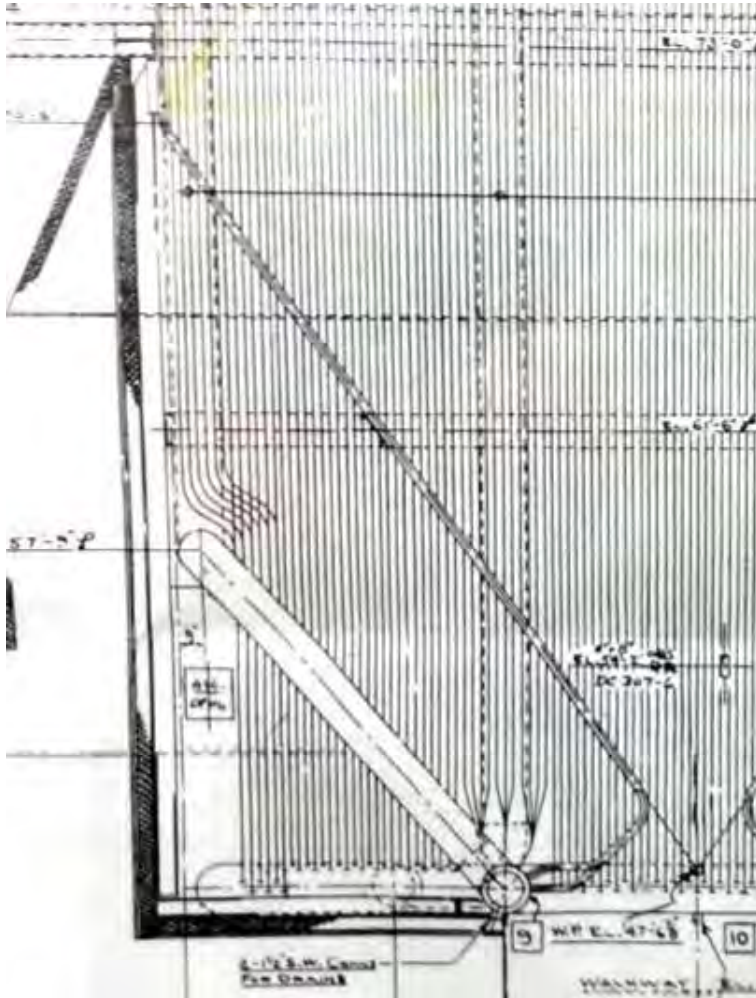
Original ISOMEMBRANE® Installation in 1994

Case Study: Lower Slope Clinker Damage

- 18' x 4' square clinker impact
- Emergency outage
- ISOMEMBRANE® installed in 3 shifts



Case Study: Lower Dead Air Space

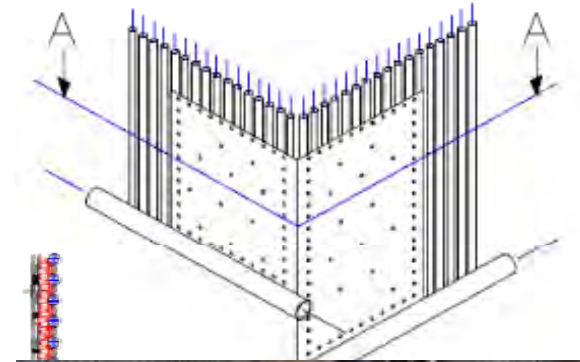


Case Study: Lower Dead Air Space

Installation prior to the ISOOCOAT[®] layer



Case Study: Stoker Furnace Corner Casing Seal



Case Study: Stoker Boiler Chill Tube Casing Irregular Surface Installation Flexibility

Before



After



Case Study: Center Waterwall Header

Before



ISOMEMBRANE® in the
4th & 5th stages of installation



Installation Considerations

- Substrate Conditions
- Understanding of Movement
- Proper Installations



ISOMEMBRANE® as a Tool

In-situ Manufactured Expansion Joints

Aging and failing expansion joints are one of the most immediate risks to power plant compliance, availability, net output and emissions.



The Real Costs of Flue Gas Path Leakage

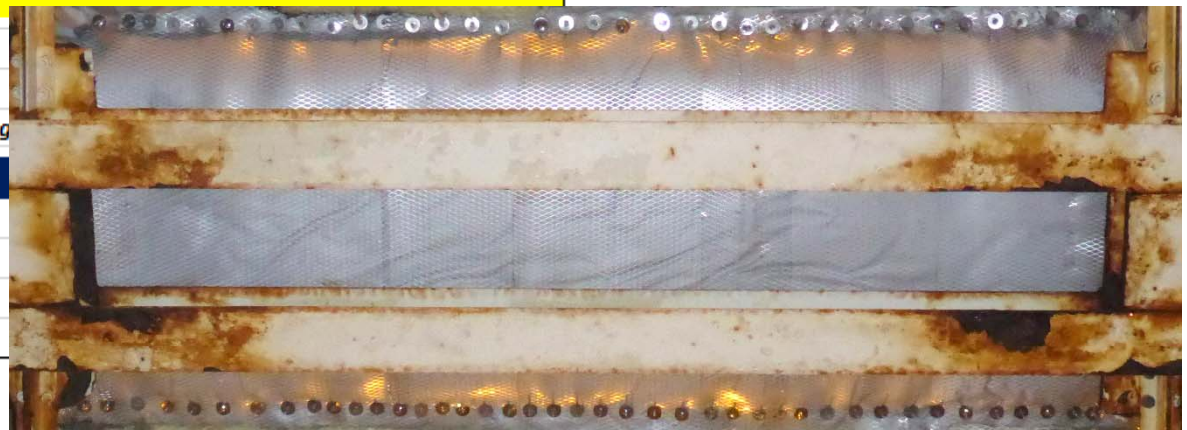
Fan ROI Calculator by Howden Fan*

FAN MOTOR ENERGY SAVINGS CALCULATOR			
Power Consumption Savings			
Horsepower	700	HP	
Voltage	4160	Volts	
Fan Power Factor	0.85	(0.85 for 3	
Current Before	64	Amps	
Current After	54	Amps	
Amp Draw Improvement	16%	Improvement	
Energy cost	8	cents/KWh	
Power Before	391.97	KW	
Power After	330.72	KW	
Power Δ	61.25	KW	
Energy (24 hrs)	1,469.89	KWh	
Plant Availability Factor	90%		
Energy (8760 hrs)	482,858.08	KWh	
Annualized Savings	\$ 38,628.65	Savings	
Project Cost	\$ 25,021.00		
ROI	236	days	
<i>Note: This ROI calculation reflects only the direct energy saving</i>			
Pressure Improvement			
Pressure Before	16	"WC	
Pressure After	12	"WC	
Recovered Pressure	4	"WC	
Improvement	25%	Improvement	

A copy of this ROI Calculator in Excel format is available from HTT

CASE: 53MW Pennsylvania waste-to-energy plant.

- In-situ manufactured expansion joint encapsulation of failed joint & corroded ductwork upstream of the baghouse inlet
- **Completed in 2 shifts, while unit online**
- **Immediate Plant Reported Results:**
 - Decrease in Fan Pressure: 16"WC to 12"WC (25% improvement)
 - Decrease in Amp Draw: 64 amps to 54 amps (16% improvement)
 - **Capacity Recovered: 1 MW**
- Value of Recovered Capacity: **\$275,520** (wholesale PJM for 2017)
- Annual savings from reduced parasitic power consumption: **\$38,625**
- **ROI: 29 days**



Case Study: ISOMEMBRANE® In-situ Manufactured Expansion Joint Encapsulations

- Unit 10: A&B APH Secondary Air Joints (2) (*Internal*)
- Unit 10: Scrubber/ID Fan Duct Joint (*Internal*)
- Unit 10: Precipitator Outlet Joints (2) (*Online*)



Case Study: A/B APH Secondary Air Joints

- External access limitations avoided *(Internal Installation)*
- Avoid demolition and refabricating the duct and flange
- In-situ manufactured joint installed in 2-2.5 shifts



Existing Corroded Metal Bellows Joint.
Expensive & time-consuming to replace.
With in-situ manufactured joint encapsulations, demolition, flange/metal repair & fabrication are not required. Nor are detailed measurements.



- *ISOMEMBRANE® bridges beyond corroded flanges & ductwork to good metal.*
- *120 linear feet per joint*
- *Both joints completed in 5 shifts*

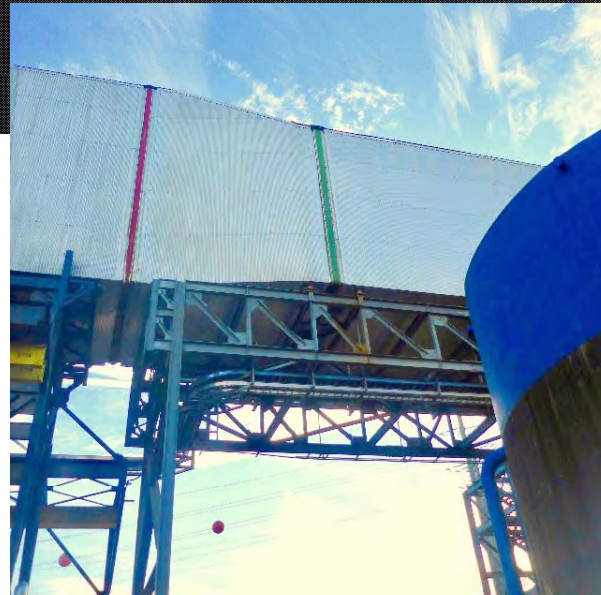
Case Study: Scrubber/ID Fan Duct Joint

(Internal Installation)

- Minimizes scaffolding requirements & costs
- Improves job-site safety

ISOMEMBRANE® INTERNAL *in-situ manufactured expansion joint encapsulation over existing fabric type joint,*

- Internal install avoided the need for expensive exterior, ground-up scaffolding
- Joint Size: 28'4" x 28'4"
- Completed in 2 shifts



Case Study: Precipitator Outlet Joints (2)

External, Online Installation

- Completed outside the outage window



ISOMEMBRANE® expansion joint encapsulation over existing joint

- *Each Joint: 113' x 48'*
- *322 linear feet per joint -744 total LF*
- *2 joints completed in 7 shifts*



Case Study: Online Installations

Safety dependent, typically negative draft / <350°F

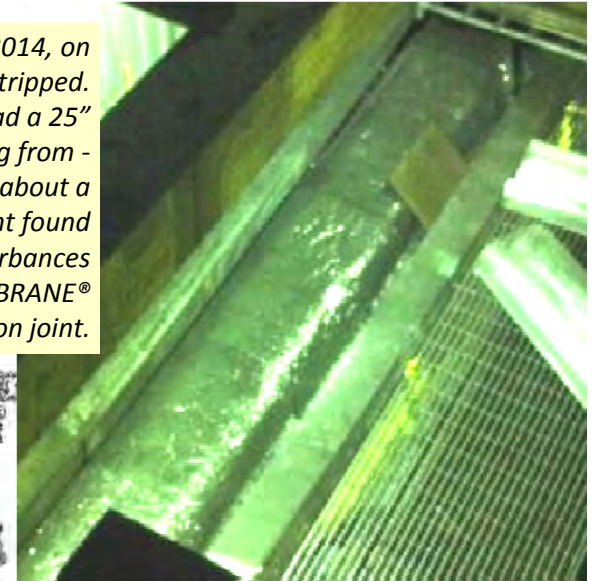
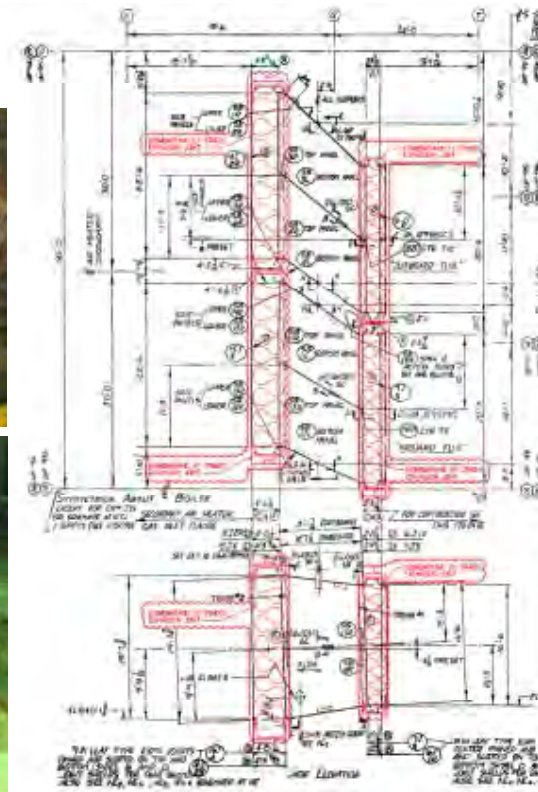
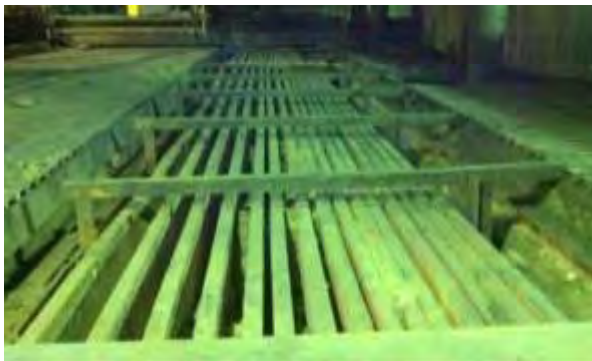
- Emergency Response:
(Can typically deploy within 12 -24 hours)
- Allows work to be completed without loss of production, minimizing job-site traffic & projects to oversee.



Case Study: Economizer Outlet Joints

- **1170MW Supercritical Unit**
- **8 Economizer Outlet Joints Per Unit**
- Operating parameters
 - Temperature: <1,200°F
 - Pressure: -15" WC
- Two sizes
 - 22' x 20' x 4.5' seal breach
 - 22' x 12' x 4.5' seal breach

NOTE: On 1/7/2014, on start-up, this unit tripped. The boiler had a 25" excursion, going from -15" to +10" in about a minute. The plant found no issues or disturbances with the ISOMEMBRANE® expansion joint.

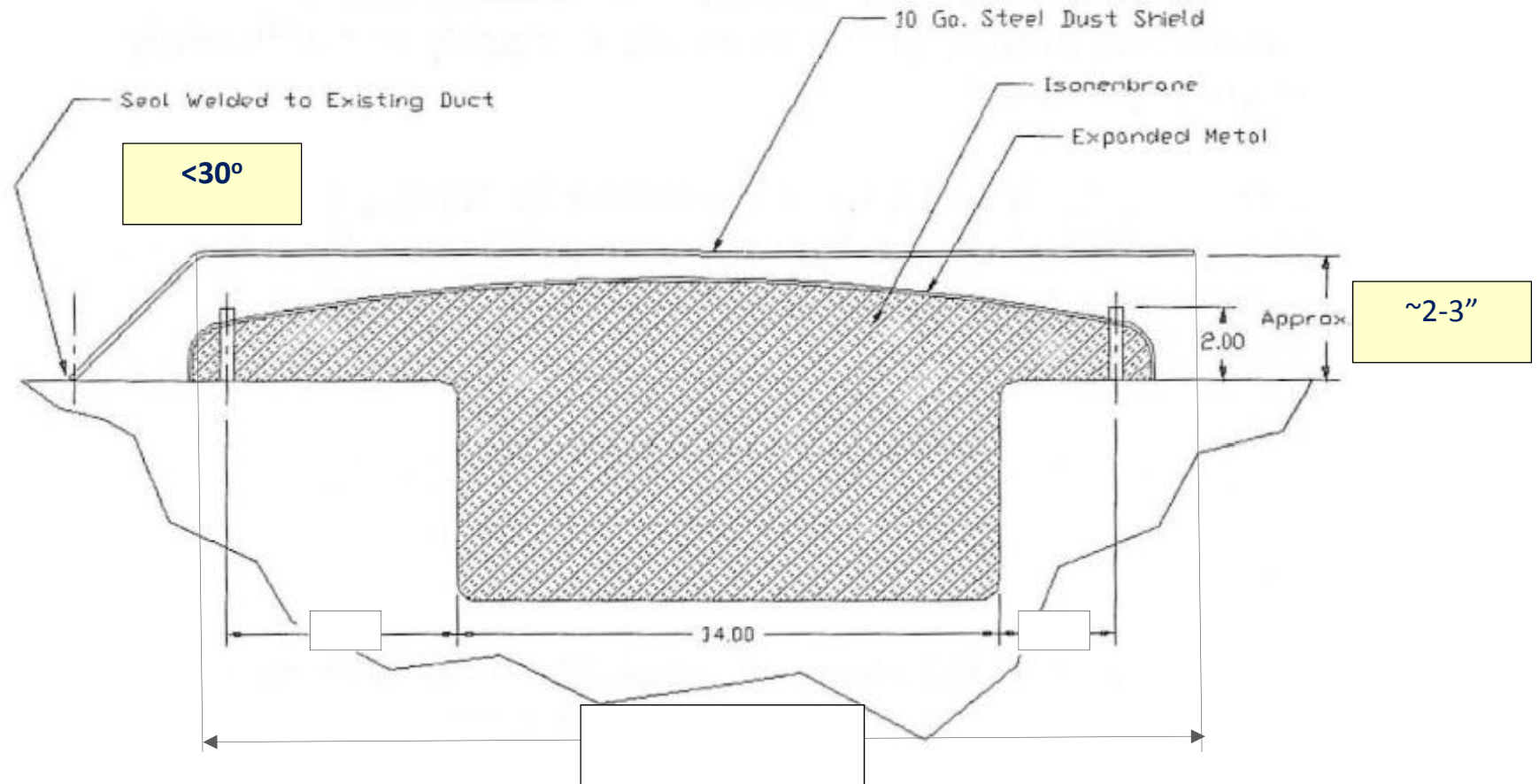


Case Study: Precipitator Outlet Joint & Flange



- 14'x14'x30" joint
- ISOMEMBRANE® installed over the joint and flange to good metal.
- Joint Flanges adjacent to joint were cracked (due to ash loading) & corroded.
- No metal fabrication was required.
- Restored fan capacity and reduced parasitic power consumption.
- ISOMEMBRANE® encapsulation was completed in 3 shifts.

Expansion Joint Shielding High Temperature Internal Encapsulation



Case Study: Internal Encapsulation

Before



After



- with flow shield



RFQ Requirements

No Detailed Pre-engineering Required

Approximate joint dimensions, temperature & pressure

Part/Location/Unit:	
Quantity:	Per Unit
Length:	ft/in
Width:	ft/in
Breach (flange to flange):	/ in./ if adjacent ductwork is corroded, approx distance to good metal beyond the flange
Movement:	inches <input type="checkbox"/>Expands or <input type="checkbox"/>Contracts at operating temperature
Temperature:	°F (approx.)
Pressure+/-:	"H₂O (approx.) <input type="checkbox"/>Negative or <input type="checkbox"/>Positive
Install Location Preference:	<input type="checkbox"/>External <input type="checkbox"/>Internal <input type="checkbox"/>Undetermined
<i>Target Install Date?</i>	
<i>Level of Urgency</i>	<i>"1" being Very High, "5" being Very Low</i>
<i>Drawings/Photos Available?</i>	

External versus Internal ISOMEMBRANE® installation:

- External – External sealing has advantages when the joint is under negative pressure; potentially lower install cost, ability to install ISOMEMBRANE® while the unit is online, and/or avoid the need for internal shielding. On positive pressure joints, this is an option when time and access are limited.)
- Internal – Internal sealing has advantages when the joint is under positive pressure; potentially lower install cost, and/or where applicable, avoid/minimize scaffolding requirements.)

ISOMEMBRANE[®] for HRSG's



HRSG Superheater Section Penetration Seals



BEFORE: This area had been problematic due to chronic cracking causing heat loss, efficiency issues and safety concerns. Standard repair methods were unreliable and required repetitive maintenance.



DURING: ISOSTUD® & ISOBLANKET® Installation.



DURING & AFTER: The final stage, the ISOCOAT® layer, is a thin layer (1/8") topcoat that enhances impermeability and protects the ISOBLANKET®)



Rooftop Penetration Seals

*2017: ISOMEMBRANE®
after 3.25 years in service*

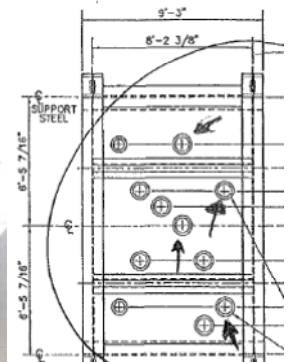


DELTA K

ISOMEMBRANE® Installation June 2014 on a Deltak unit where high heat from leaking roof penetrations damaged controls nearby causing the unit to trip twice.

The ISOMEMBRANE® installation on 8 penetrations was completed in 2 shifts while unit was offline for the weekend.

The plant manager reported the OEM type repairs would have required 7 shifts at almost twice the price.



Rooftop Penetration Seals

Installation Stage 9 of 14 stages



Rooftop Penetration Seals

Installation Stage 9 of 14 stages



Rooftop Penetration Seals



Downcomer Roof Tube Penetrations



Roof Tube Penetrations



Header Drain Tube Penetrations





Exhaust Expansion Joints

High Temperature – High Pressure

Before



After



Exhaust Expansion Joints



High Temperature – High Pressure

Before



After



Exhaust Expansion Joints

High Temperature – High Pressure

Before



After



Stack Expansion Joints

ISOMEMBRANE®: Faster to Install, Less Expensive





Fan & Boiler ROI Calculators (Excel)

Fan ROI Calculator by Howden

Boiler ROI Calculator by ICT

FAN MOTOR ENERGY SAVINGS CALCULATOR		
Power Consumption Savings		
Horsepower	700	HP
Voltage	4160	Volts
Fan Power Factor	0.85	(0.85 for 3-Phase Electric Motor, 1
Current Before	64	Amps
Current After	54	Amps
Amp Draw Improvement	16%	Improvement
Energy cost	8	cents/KWh
Power Before	391.97	KW
Power After	330.72	KW
Power Δ	61.25	KW
Energy (24 hrs)	1,469.89	KWh
Plant Availability Factor	90%	
Energy (8760 hrs)	482,858.08	KWh
Annualized Savings	\$ 38,628.65	Savings
Project Cost	\$ 25,021.00	
ROI	236	days

Note: This ROI calculation reflects only the direct energy savings for the electric motor.

 The Boiler ROI calculator was created for HTT by INNOVATIVE COMBUSTION TECHNOLOGIES (ICT). ICT specializes in addressing combustion side parameters to identify & explore opportunities for improved unit heat rate, performance, availability, capacity and operability.						
 High Temperature Technologies, Inc. 4324 Barringer Drive #107, Charlotte, NC 28017 704.375.2111 www.isomembrane.com Patrick Fitzgerald cell: 704.621.2465 patrick@isomembrane.com						
Yellow Boxes are for manual data entry. Other fields self compute.						
For a copy of this BOILER ROI Calculator (in Excel format), email me, and I'll send you a copy. patrick@isomembrane.com						
ROI Calculator - Air In-Leakage Control						
Unit Net Load (Mw)	788	Hours/yr	6570			
Availability	75%	Capacity Factor	56%			
Number of ID Fans	2	Fan HP	1,800			
Heat Rate (Btu/Kwhr)	10,500	Heat Rate (Btu/Mwhr)	10,500,000			
Fuel Cost (\$/ton)	50	Fuel Heating Value (HHV) Btu/lb	12,000			
Calculations:						
Mw/yr	3882870 Total Mw's					
Mw/yr = Unit Net Load (Mw) * Cap Factor (%) * 365 (days/yr) * 24 (hrs/day)						
Fuel Cost	\$ 2.08 \$/M-Btu					
\$/M-Btu = Fuel Cost (\$/ton) * 1000.0001 (HHV (Btu/lb) * 2000 (lb/ton))						
\$/Mwhr = (Heat Rate (Btu/Mwhr) * Fuel Cost (\$/ton)) / (Heating Value (Btu/lb) * 2000 (lb/ton))						
Parameter	Quantity or %Change in Heat Rate	Cost or Penalty	Total Cost Savings (per Year)	Savings LOW	Savings HIGH	
FLYASH LOSS ON IGNITION (LOI) (alternative way of looking at fuel savings)	1% Reduction in LOI	10.50 Btu/Kwhr	\$ 84,938	\$ 84,938		
(Assume 0.1% Heat Rate per 1% LOI)	2% Reduction in LOI	21.00 Btu/Kwhr	\$ 169,876		\$ 169,876	
LOST GENERATION						
Occurrences/yr	Hours/occ	\$/Mwhr				
Lost Generation (54Mw de-rate to shed furnace slag)	1	8	\$35	\$ 220,640	\$ 220,640	
Lost Generation (54Mw de-rate to shed furnace slag)	2	8	\$35	\$ 441,280	\$ 441,280	
Lost Generation (Unit off-line due to slagging incident, [x] 3-day incidents/yr)	1	72	\$35	\$ 1,985,760	\$ 1,985,760	
Lost Generation (Unit off-line due to slagging incident, [x] 3-day incidents/yr)	2	72	\$35	\$ 3,971,520	\$ 3,971,520	
Plus fuel oil for restarts						
REDUCED AUXILIARY HORSEPOWER FOR ID FANS						
(Repair resulted in decrease in mass flow of 4% yielding 7% reduction in ID HP of 10%)	180.00	# ID Fans * Capacity Factor * HP Reduction * 7455 Kw * Yearly Hours	\$0.045 Kw/Hr Bus Bar cost	\$ 43,641	\$ 43,641	
(Repair resulted in decrease in mass flow of 8% yielding 14% reduction in ID HP of 20%)	360.00	# ID Fans * Capacity Factor * HP Reduction * 7455 Kw * Yearly Hours	\$0.045 Kw/Hr Bus Bar cost	\$ 87,281	\$ 87,281	
DE-SUPERHEATING SPRAY FLOWS (SH) Assume 0.025% Heat rate for 1% of MSF						
De-superheating Spray Flows (SH) Assume 0.025% Heat rate for 1% of MSF	1	1% MSF Sprays Reduced	2.63 Btu/Kwhr	\$ 21,234	\$ 21,234	
De-superheating Spray Flows (SH) Assume 0.025% Heat rate for 1% of MSF	2	2% MSF Sprays Reduced	5.25 Btu/Kwhr	\$ 42,469	\$ 42,469	
DE-SUPERHEATING SPRAY FLOWS (RH) Assume 0.2% Heat rate for 1% of MSF						
De-superheating Spray Flows (RH) Assume 0.2% Heat rate for 1% of MSF	1	1% MSF Sprays Reduced	21.00 Btu/Kwhr	\$ 169,876	\$ 169,876	
De-superheating Spray Flows (RH) Assume 0.2% Heat rate for 1% of MSF	2	2% MSF Sprays Reduced	42.00 Btu/Kwhr	\$ 339,751	\$ 339,751	
REDUCED BOILER EXIT GAS TEMPERATURE (.25% change in heat rate per 10°F)						
		10 °F Reduction	26.25 Btu/Kwhr	\$ 212,344	\$ 212,344	
		20 °F Reduction	52.50 Btu/Kwhr	\$ 424,689	\$ 424,689	
COST OF FUTURE MAINTENANCE ACTIVITIES AVOIDED						
	Low	High				
Penhouse Vacuuming	\$ 20,000	\$ 40,000				
Refractory Redo/Repairs	\$ 20,000	\$ 40,000				
Penhouse casing/penetration weld repairs	\$ 20,000	\$ 40,000				
			Fully Loaded Total		\$ 2,798,433	\$ 5,596,866

Please provide email address for the ROI Calculators & copy of this presentation.

Other Reference Documents:

- * ISOMEMBRANE® Sealing Project Report
- ** BOILER ROI Calculator to estimate savings associated with air in-leakage, created by Innovative Combustion Technologies.
- *** 2017 EPRI Heat Rate Conference Paper, "Impact of Air In-Leakage on Unit Reliability & Operating Costs," by Stephen Storm, Duke Energy's Combustion & Boiler Performance Program Manager, and Patrick Fitzgerald, High Temperature Technologies.





2019 UDC 24th Annual Users Conference

Controlling Air In-Leakage to Optimize Unit Performance & Reliability, and Reduce Operating Costs



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2019 NOx-Combustion-CCR/PCUG Conference

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